

The effect of power cycles architectures at hydrogen production plants

First step of analysis

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1 The goal

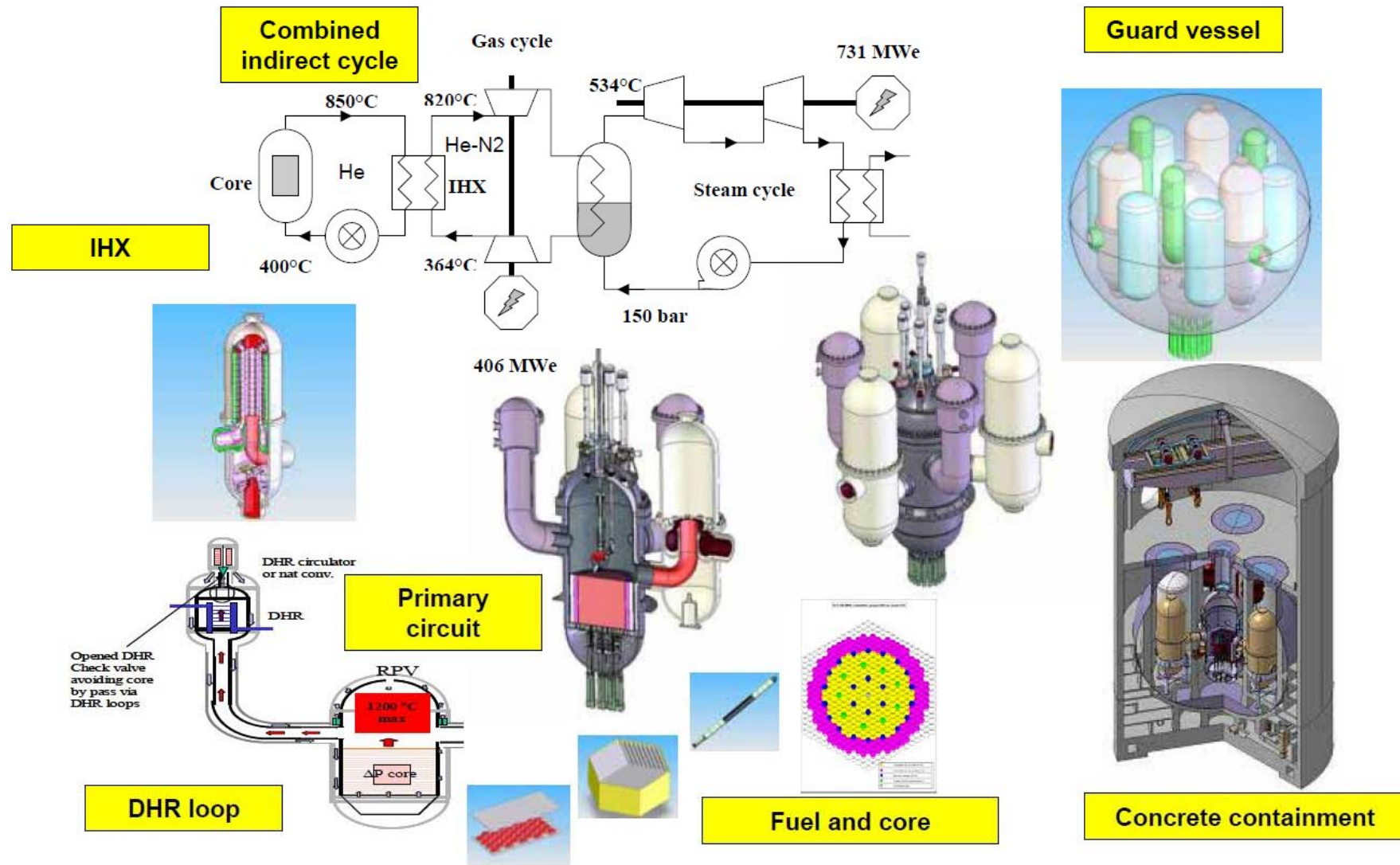


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- The main goal of this information is to prepare basis for optimization of high temperature H₂ production in connection with HTR and VHTR.
 - It is also necessary to find the criteria for optimization .
 - Short comments about CEA activities at the area of High temperature reactors

2 Gas Fast Reactors



■ The CEA's 2007 GFR Reference Concept – 2400 MWth Reactor



2 Gas Fast Reactors



The CEA's 2007 GFR Reference Concept COMMENTS:

- **Main supposed advantages:**

- no activated coolant
- appropriate efficiency more than 40%

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- **Main supposed problems:**

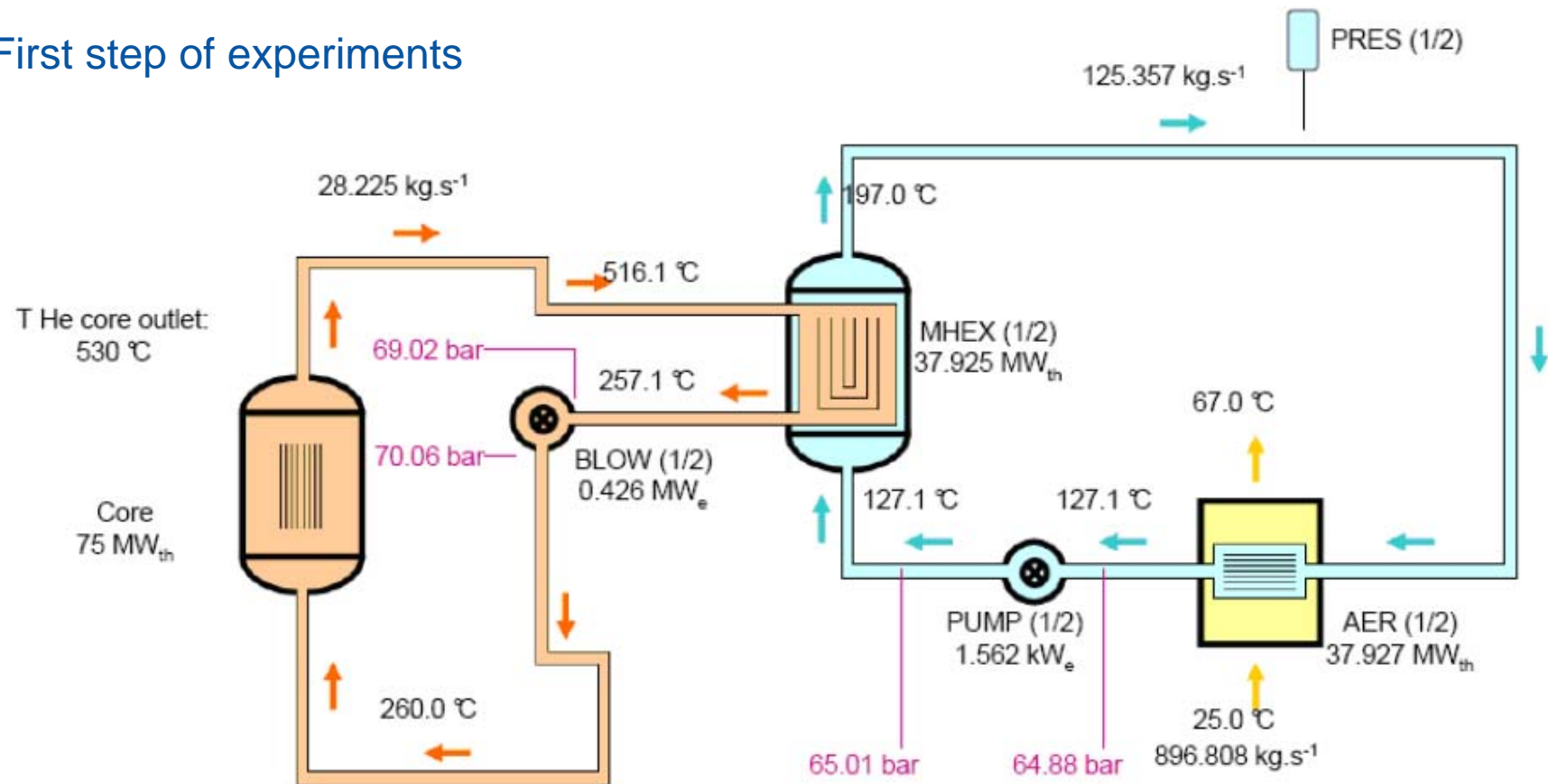
- very high temperatures
- material problems
- - fuel, fuel manipulation
- - safety
- He is very bad coolant (in comparison with water, liquids metals)
- **GFR concept has no connection to the hydrogen production**
- **CEA all activities at GFR stopped**

3 Allegro



.The CEA's GFR experimental reactor – 75 MW_{th} Reactor

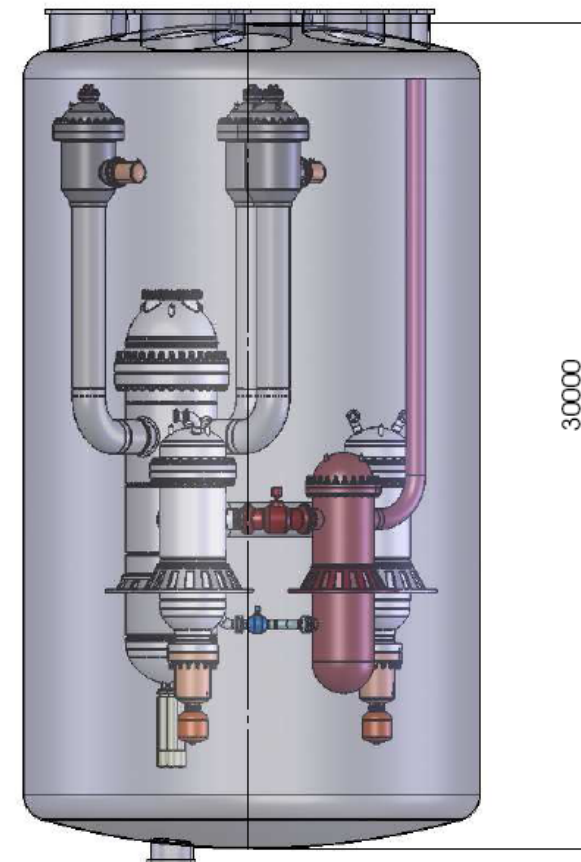
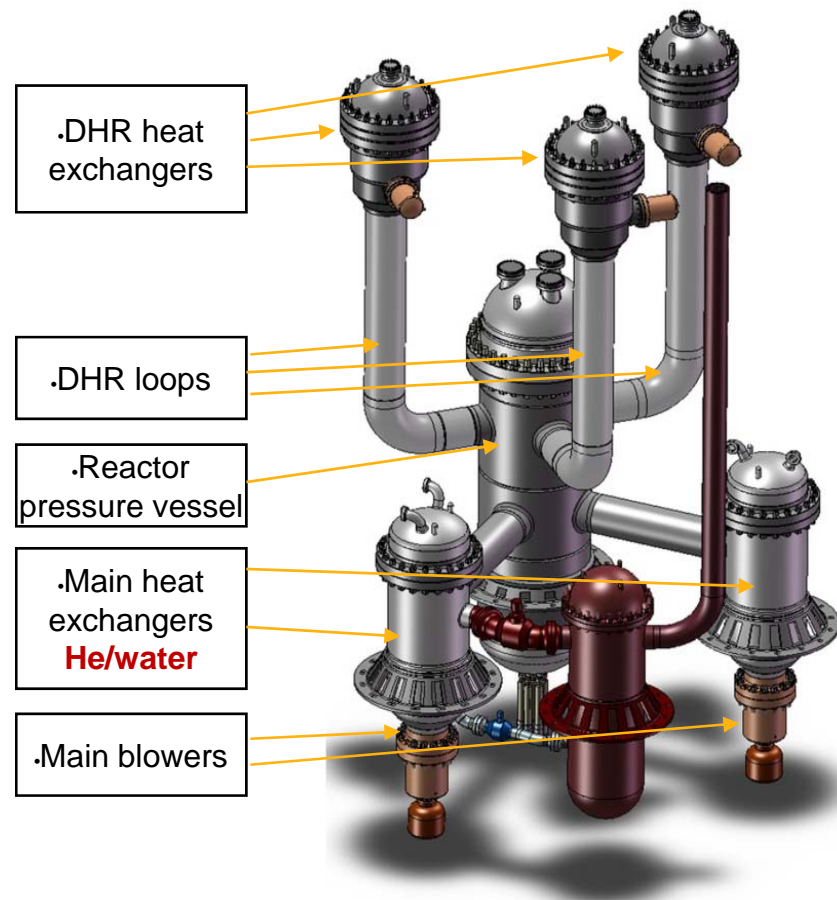
.First step of experiments



3 Allegro



.The CEA's GFR experimental reactor – 75 MWth Reactor



3 Allegro



The CEA's GFR experimental reactor – 75 MWth Reactor

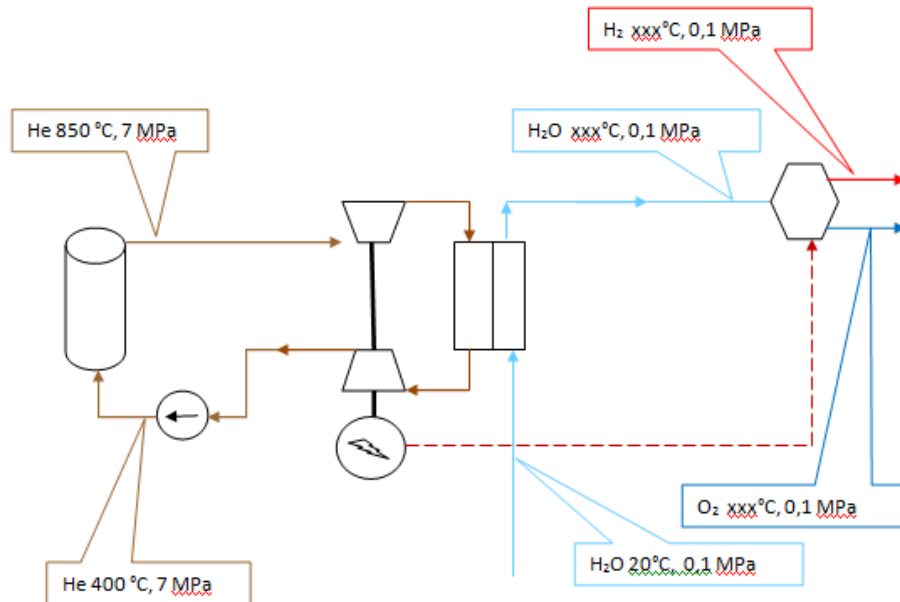
COMMENTS:

- Allegro has no conversion systems
- At this project is secondary coolant water
- The operation with MOX has no sense for hydrogen production

4 Conversion cycles



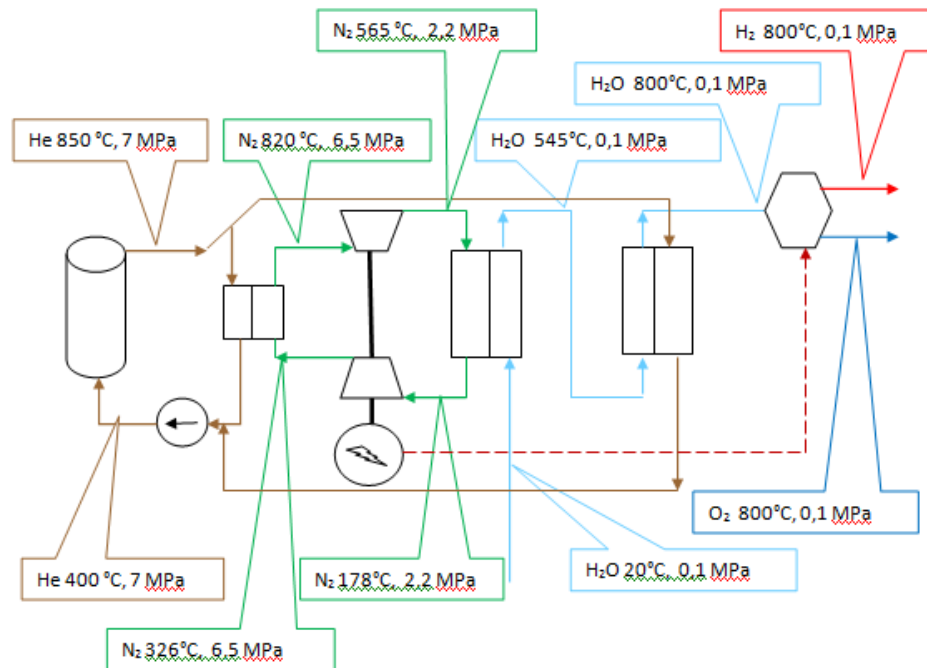
Schema 0



- .Direct Brayton cycle, without regeneration
- .Not acceptable solution, safety, contamination

4 Conversion cycles

Schema I



- Indirect Brayton cycle, without regeneration
- Realistic and acceptable solution

3 Allegro



H₂O – Hélium (3výměník)-protiproudý

	H ₂ O	Hélium
G,kg/hod	0,5	0,221
P,MPa	0,101	7
T _{in} /T _{out} ,C	545/800	850/600
L(délka výměníku),m	~1,042	
Počet trubek	1	9
Průměr trubky,m	0,1	0,004/0,006

H₂O – Nitrogen (2výměník)-protiproudý

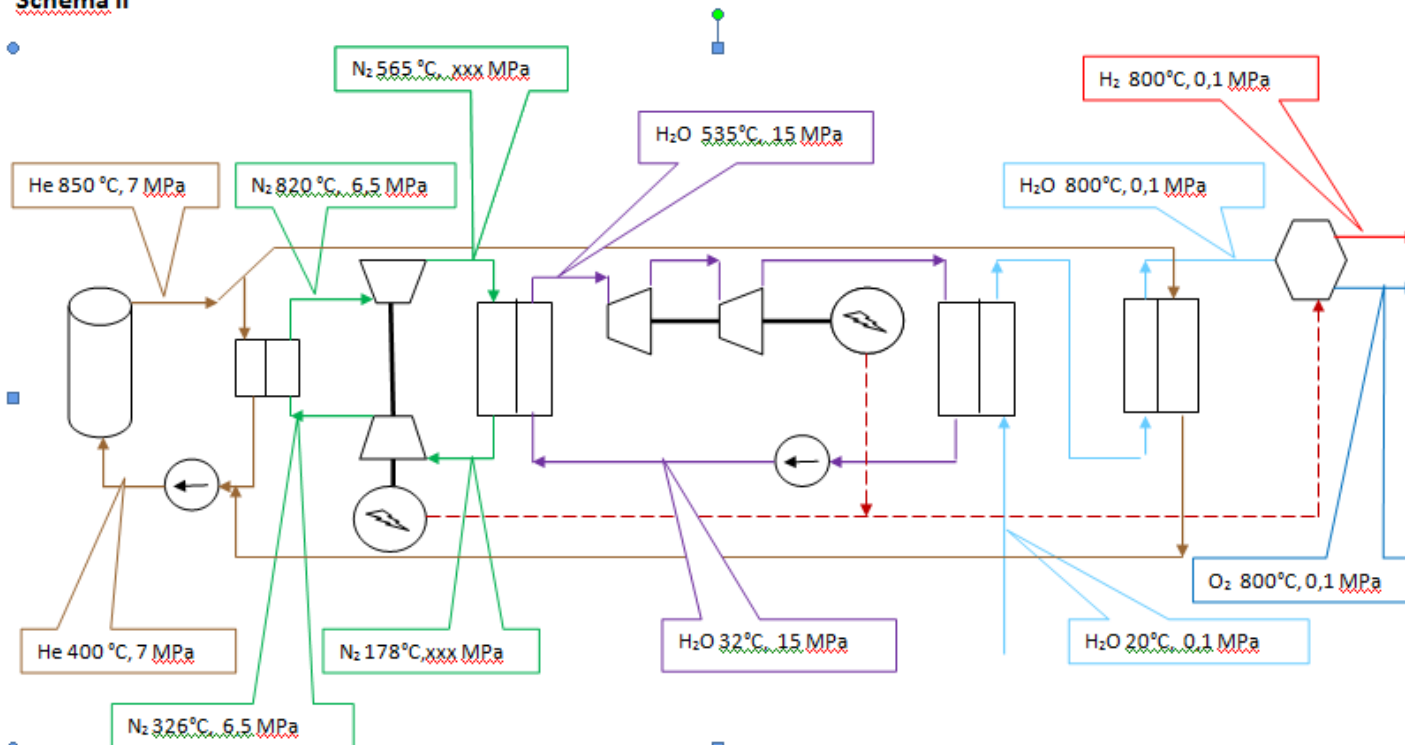
	H ₂ O	Nitrogen
G,kg/hod	0,5	4,208
P,MPa	0,101	2,2
T _{in} /T _{out} ,C	20/545	565/178
L(délka výměníku),m	~1,13	
Počet trubek	1	44
Průměr trubky	0,1	0,004/0,006

Nitrogen – Hélium (1výměník)-protiproudý

	Nitrogen	Hélium
G,kg/hod	4,208	1,83
P,MPa	6,5	7
T _{in} /T _{out} ,C	326/820	850/600
L(délka výměníku),m	~0,92	
Počet trubek	1	12
Průměr trubky	0,1	0,004/0,006

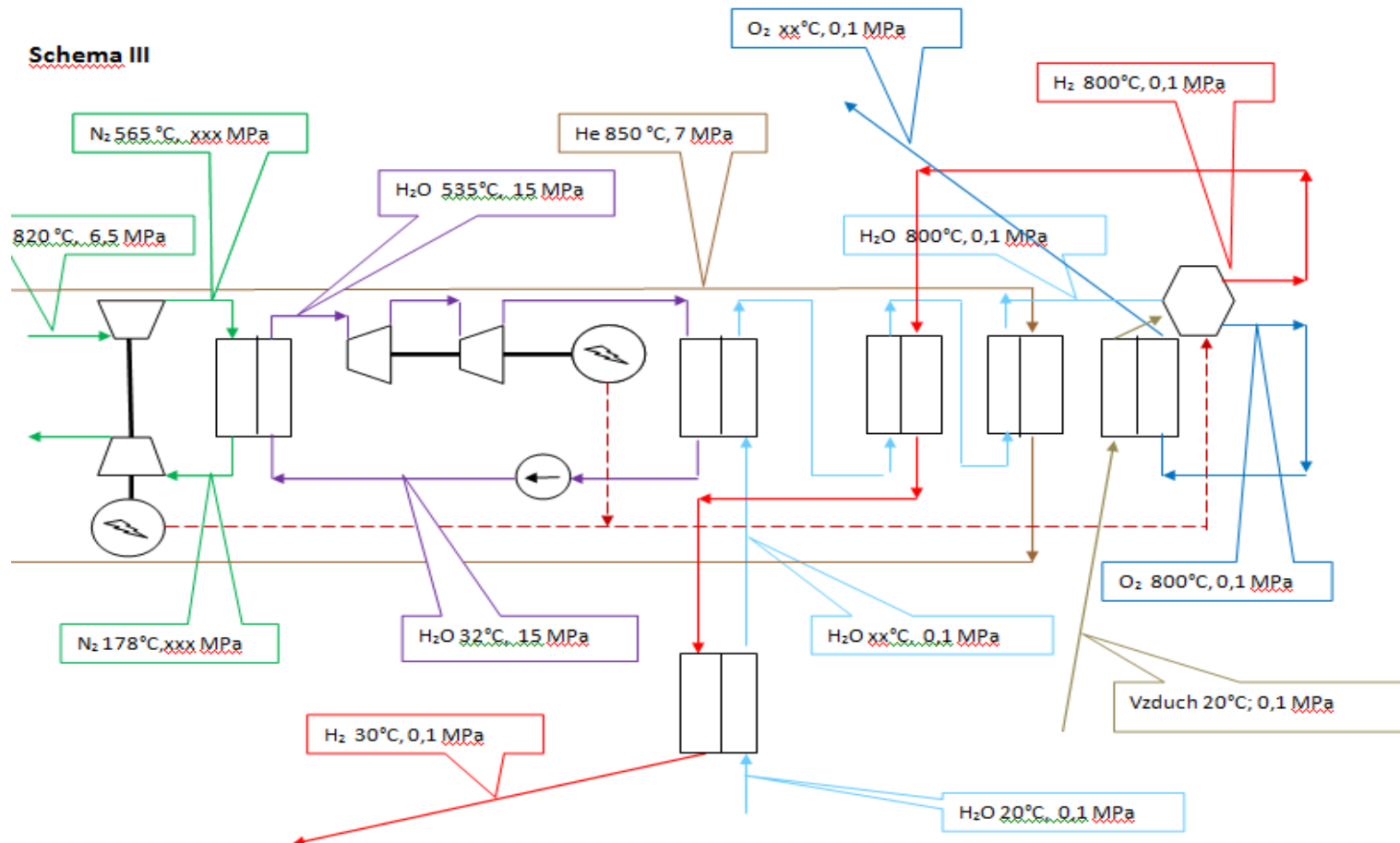
4 Conversion cycles

Schema II



- Combined cycle, without regeneration
- Necessary growth of lower temperature of steam cycle, loss of efficiency

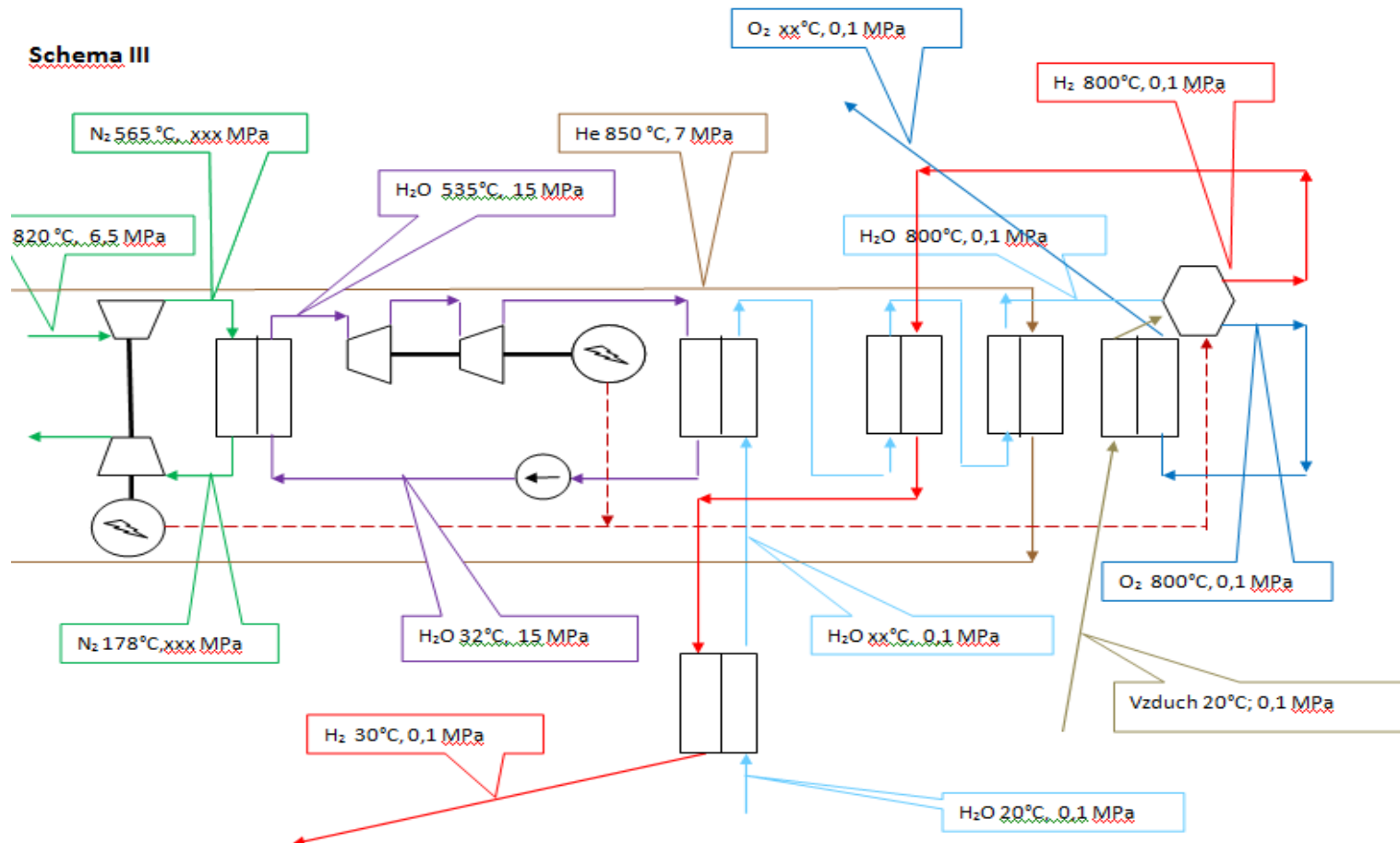
4 Conversion cycles



.Combined cycle, with regeneration

.Necessary growth of lower temperature of steam cycle, loss of efficiency

4 Conversion cycles

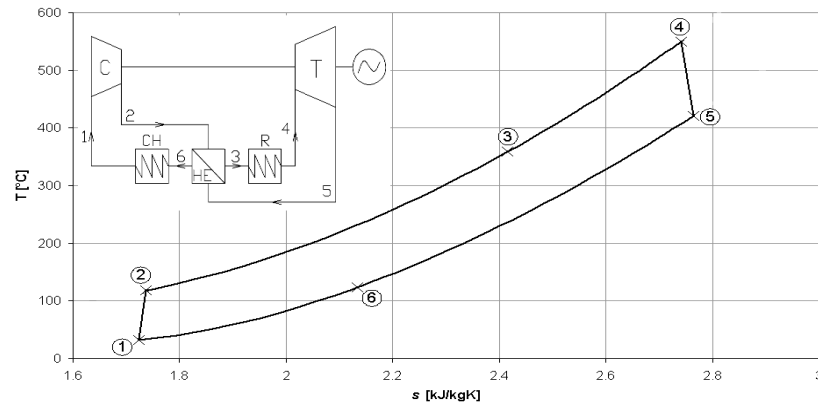


.Combined cycle, with regeneration

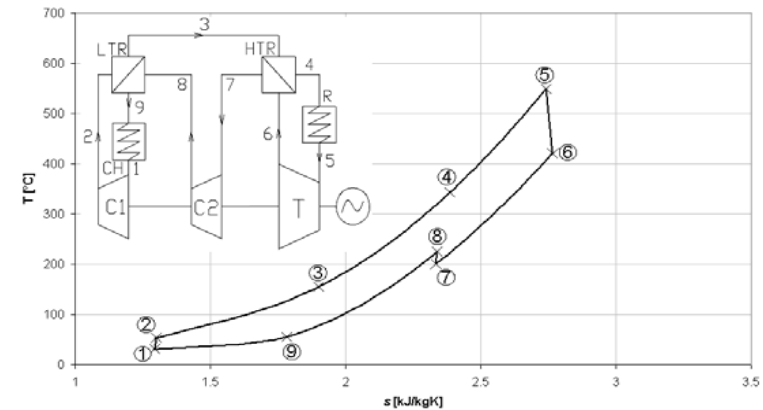
.Necessary growth of lower temperature of steam cycle, loss of efficiency

4 Conversion cycles

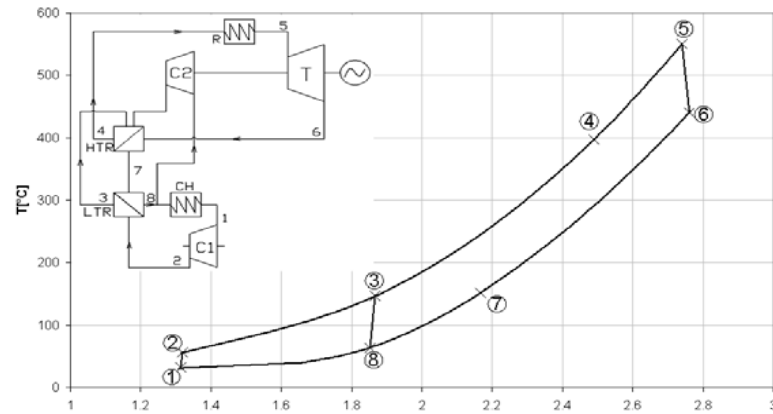
.Simple Brayton (A)



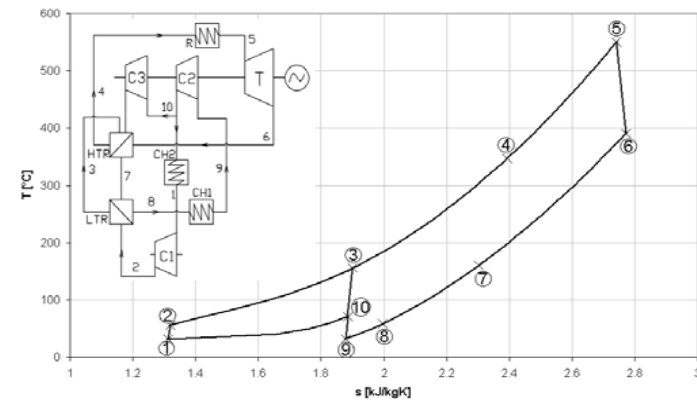
.Pre-compression (B)



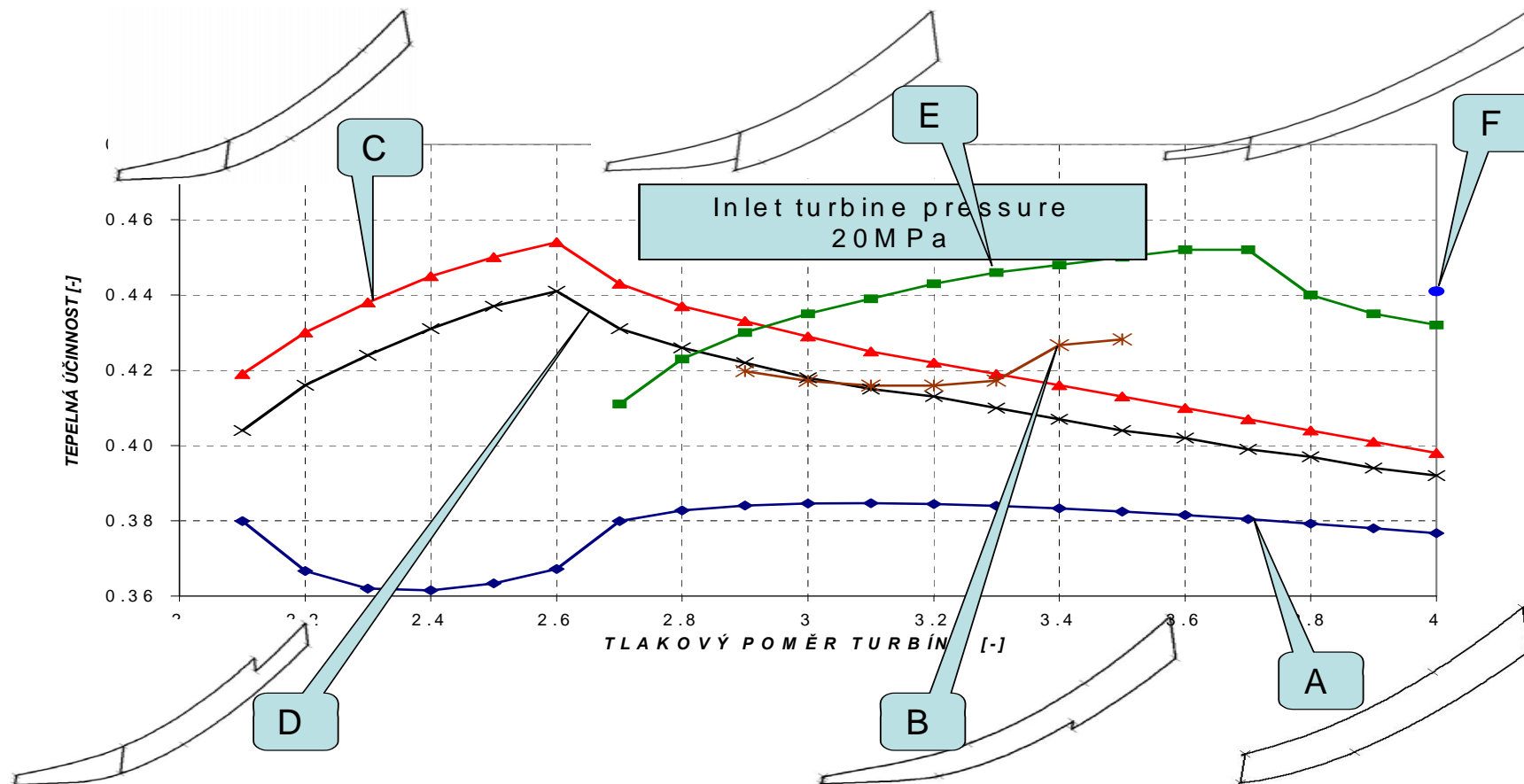
.Re-compression (C)



.Partial Cooling Cycle (E)



4 Conversion cycles

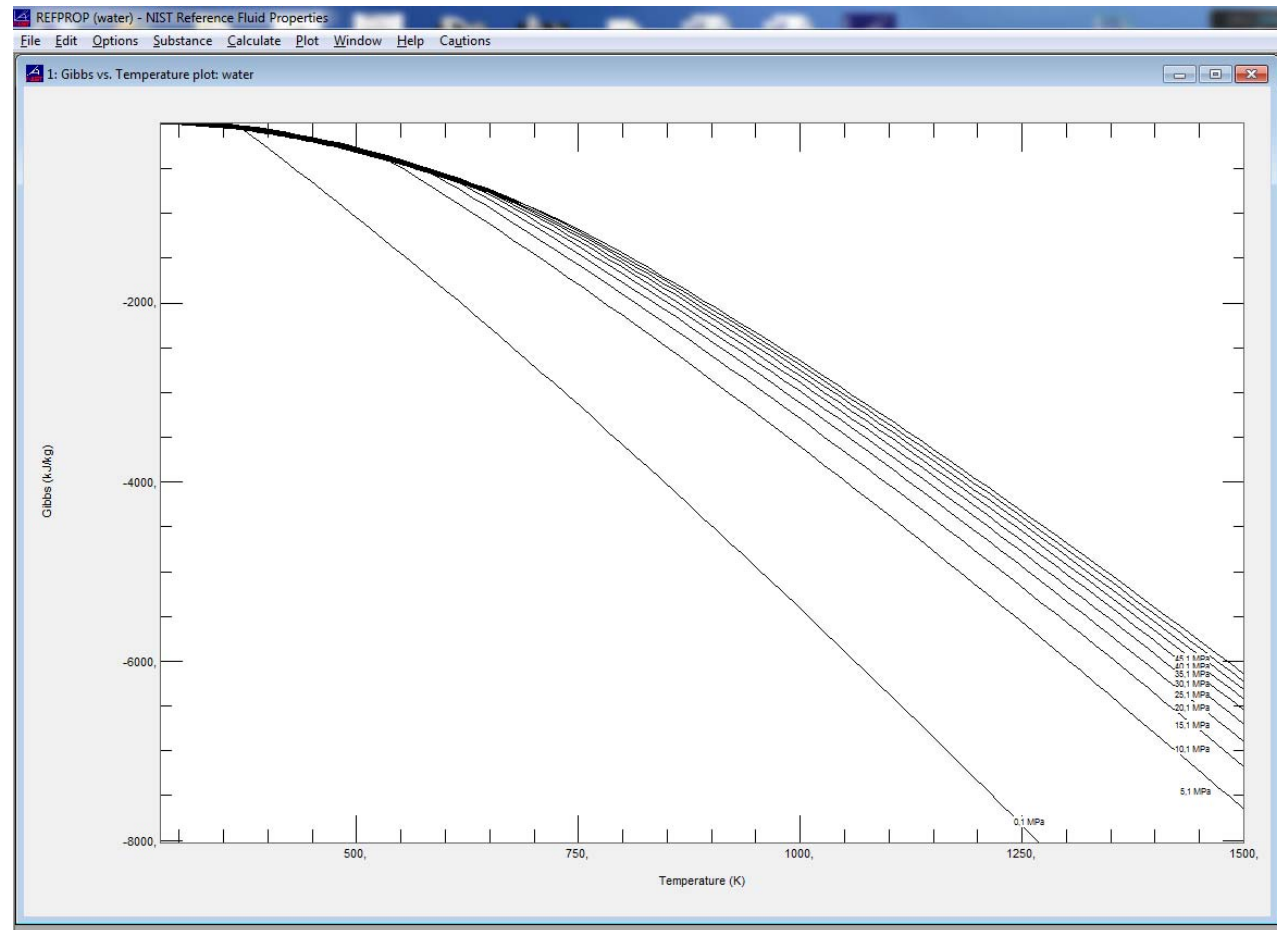


Important difference to the steam cycle – no one cooling temperature

5 High temperature electrolysis



.The reduction of electricity consumption is done by Gibbs energy



6 Main criteria



.The input parameters:

- pressure and mainly temperature of GFR

.The output parametrs:

- pressure and temperature of hydrogen

.The internal paramentrs

- Cycle architecture
- Used media
- Paramemers of media (pressure, temperature)

.Optimal output – no losses at GFR (no cooling), no additional electric power

7 Next steps



- .The final list of conversion cycles**
- .The SW connected with NIST**
- .Results evaluation**
- .Cycles optimization (for example minimum of HX etc.)**

8 Conclusions



- .The developement of GFR is today freezed**
- .The defect connection with H2 production can lead to to new steps in R&Dof GFR**
- .Suggested GFR architecture (combined cycle) is not ideal for SOEC**
- .The finalyizing of the architectures optimization is important next steps**
- .Also the developement of SOEC of great power in importatnt step**

Thank you for attention